wull8/2/2

FUEL RESEARCH INSTITUTE OF SOUTH AFRICA.

TECHNICAL MEMORANDUM NO. 33 OF 1965.

REPORT ON THE RESULTS OBTAINED FROM AN ACCEPTANCE TEST CARRIED OUT ON THE COAL PREPARATION PLANT AT PHOENIX COLLIERY, BEATH SECTION.

BY:

S.F. STREICHER

FUEL RESEARCH INSTITUTE OF SOUTH AFRICA.

TECHNICAL MEMORANDUM NO. 33 OF 1965.

REPORT ON THE RESULTS OBTAINED FROM AN ACCEPTANCE TEST CARRIED OUT ON THE COAL PREPARATION PLANT AT PHOENIX COLLIERY, BEATH SECTION.

INTRODUCTION:

The F.R.I. was requested by the Metalurgical Manager, Contracts Division, Fraser and Chalmers (S.A.) (Pty.) Ltd. to conduct an acceptance test on the newly commissioned Wemco Drum washer at Phoenix Colliery, Beath Section, on behalf of Johannesburg Consolidated Investment Co. Ltd.

OBJECT OF THE TEST:

The object of the test was to determine the efficiency of separation in the drum under full load conditions over a period of at least five hours. This entailed:

- (a) Sampling the products from the washer at predetermined intervals over the test period.
- (b) Determining the total input to the plant at regular intervals.

THE TEST:

The test was carried out on Tuesday, June 15, 1965 and was started at 9 a.m. Because the total input to the plant under full load conditions exceeded the total underground output of the colliery, sampling had to be interrupted for 1 hour at 12 noon in order to allow the stock pile to build up sufficiently for the test to be continued. At 2.30 p.m., however, reserves were again so low that it was decided to stop the test rather than continue under reduced load conditions. The total test period was therefore reduced to $4\frac{1}{2}$ hours.

The Wemco drum is designed to treat 6" x $\frac{3}{8}$ " coal, but in view of the excessive weights of samples that would have to be taken when the +4" material is included, it was decided by mutual consent of the parties concerned, that analysis would only be carried out on the -4" size

fractions.

Washing efficiencies invariably decrease with dimmishing size ranges treated, so that it follows that if the washer could meet the overall guarantee with the exclusion of the +4" size fraction, it must have done more than fulfill the overall guarantee.

LOAD TEST:

As no weightometer was available for weighing the raw coal feed to the plant, the load was determined by stopping the raw coal feed belt at 20 minute intervals and by clearing exactly 3 ft. of the conveyor and by weighing the increment obtained. The speed of the raw coal conveyor was determined under full load conditions and was found to be 324 ft. per minute. Results of these load determinations are reported in Table 1.

SAMPLING:

A. Raw Coal:

The increments obtained from the load determinations were screened at 4" and combined for use as a raw coal sample.

B. Washery Products:

Samples of clean coal and discard were obtained by taking increments (of approximately 100 lb.) at 5 min. intervals over the entire widths of the relevant draining, rinsing and dewatering screens. These samples were also screened at 4" on site.

After screening the samples were collected in grain bags and transported to the laboratories of the F.R.I. in Pretoria where they were analysed.

C. Medium in Circulation and Magnetic Separator Underflow:

Samples of the "correct density" medium in circulation and of the underflow from the magnetic separator were taken at 10 min. intervals over the test period.

ANALYSIS OF SAMPLES:

On arrival at Pretoria the samples of raw coal and washery products were air-dried, weighed and screened at $2\frac{1}{2}$ ", $\frac{7}{8}$ " and $\frac{3}{8}$ " (square holes). Results of these screen analyses are reported in Table 2.

RAW COAL:

Representative sub-samples of the different size fractions arising from the screen analysis were prepared for whole coal ash analysis.

CLEAN COAL AND DISCARD:

Representative sub-samples of all the size fractions except the $-\frac{3}{8}$ " size fractions of these products were subjected to detailed float and sink analyses on a fractional basis, at 0.02 intervals in the specific gravity range 1.54 to 1.74. Results of these analyses are reported in Tables 3 - 5.

Whole coal ash analyses were also carried out on representative sub-samples of all the different size fractions of these products.

MEDIUM AND MAGNETIC SEPARATOR UNDERFLOW:

The specific gravity of the medium sample was determined and the magnetic material content and screen analysis of the solids were determined. On the magnetic separator underflow the solids content and the percentage of magnetic material in the solids were determined.

These results are reported in Table 7.

YIELDS OF PRODUCTS:

As no facilities for the weighing of the raw coal and washery products were available the yields for the different separations had to be calculated from ash balances.

EVALUATION OF RESULTS:

Using the yield values obtained from the ash balances together with the float and sink data in Tables 3-5, the analyses of the feed for the different separations were reconstituted and distribution factors were calculated. These results are also reported in Tables 3-5.

Distribution curves were then drawn for each separation (Figures l-3) and from these curves the specific gravity of separation for each size fraction was determined and probable errors were calculated. The weights of misplaced material in the products (calculated as a percentage of the feed) were also determined.

A summary of plant performance data is given in Table 6.

PRETORIA. 23rd July, 1965.

S.F. STREICHER.
PRINCIPAL TECHNICAL OFFICER.

TABLE 1.

LOAD DETERMINATIONS.

TIME	WEIGHT OF INCREMENT 1b.	CALCULATED FEED T.P.H.
9.00	109.5	354.8
9.20	123.5	400.1
9.40	113.5	367.7
10:00	109.5	354.8
10.20	121.5	393.7
10.40	130.5	422.8
11.00	114.5	371.0
11.20	119.0	385.6
11.40	112.0	362.9
13.20	111.0	359 .6
13.40	107.5	348.3
14.00	98.0	317.5
14.20	78.0	252.7
AVERAGE	commence account annual delibrate/shift desidua account alternia graphy desirate desidua graphy service.	360,9

SCREEN ANALYSIS OF RAW COAL AND PRODUCT SAMPLES.

	A	RAW COAL		CL	CLEAN COAL			DISCARD	
SIZE		YIELD			YIELD			YIELD	
	WEIGHT lb.	FRACT.	CUM.	WEIGHT lb.	FRACT.	CUM.	WEIGHT 16.	FRACT.	CUM.
4" x 2½"	246.75	18.93	18.93	1858.25	34.72	34.72	1080.25	30.24	30.24
22 x //8"	534.0	40.97	59.90	2522.25	47.13	81.85	1775.75	49.72	79.96
×	209.25	16.06	75.96	711,25	13,29	95.14	526.75	14.75	94.71
2 m	310.0	23.79	99.75	251.0	4.69	99.83	186,25	5.21	99.92
Toss	3.25	0.25		9.25	0.17		2.75	0.08	
TOTAL	1303,25	100.00	1.00.00	5352.0	100.00	100.00	3571.75	100.00	100.00

FLOAT AND SINK ANALYSIS OF THE -4" +2\frac{1}{2}" SIZE FRACTION.

	CLEAN	CLEAN COAL	DIS	DISCARD	RECONSTITUTED FEED	ITUTED	
SPECIFIC GRAVITY	YIELL	LD	XIELD		YIELL	TD	DISTRIBUTION FACTOR
	FRACT.	CUM.	FRACT.	cum.	FRACT.	CUM.	
1.54 1.54 1.56 - 1.56 1.62 - 1.62 1.62 - 1.62 1.64 - 1.64 1.70 - 1.68 1.72 - 1.72 1.72 - 1.72	92.07 11.00.05 0.05 0.05 0.05 0.15	74666666666666666666666666666666666666	00000000000000000000000000000000000000	6666 6666 667 667 677 678 678 678 678 67	8 24 20 20 20 20 20 20 20 20 20 20	883 883 889 900 900 900 900 900 900 900 900 900	10000874 10004000001 4700000
TOTAL	100,00	100,00	100,00	100.00	100.00	100.00	

TABLE 4.

	M.yer-100200000-100-177-17-1	**********		gg=211111111111	*******	*******		******		****	*****			******	*********	
FRACTION.	DISTRIBUTION FACTOR				2	$\overset{\bullet}{\circ}$	-	0	49.0	•	0		9	0		
SIZE FRA	TTUTED	TD	CUM.	6.3	8.4	0.7	2,2	2.6	83.60	4.5	5.6	9.9	7.3	8.6		100.001
1 + 1/8 II	RECONSTITUTED FEED	YIELL	FRACT.	4		. 16	- 0		1.00	0		9	10.	- 0		100.001
OAT AND SINK ANALYSIS OF THE -2	DISCARD	OI:	cum.	00	4.	9.	4.	rŮ.	∞	3.0	8.7	4.3	0	4.8		99.99
		YIELD	FRACT.	00	5	S		0	2.98	Š	-	5	9.	0	<u></u>	66.66
	CLEAN COAL	COAL	CUM.	1.5	4.0	6.7	8.4	8.6	99.21	9.4	9	9.6	9.6	9,00		100.02
		CLEAN	YIEUD	FRACT.	91.57	4.	9	-	<u>-</u>	5	2	0	0	0,	# 	S
IA		SPECIFIC GRAVITY		54	.54 - 1.5	.56 - 1.5	.58 - 1.6	.60 - 1.6		.46 - 1.6	.66 - 1.6	.68 - 1.7	.70 - 1.7	.72 - 1.7	S.1.74	TOTAL

FLOAT AND SINK ANALYSIS OF THE $-7/8" + \frac{3}{8}"$ SIZE FRACTION.

	DISTRIBUTION FACTOR		08880722211 128712120421 16844738120	
ITUTED	OI OI	CUM.	74 76 80 80 90 94 84 86 96 98 98 98 98 98 98 98 98	100.001
RECONSTITUTED FEED	YIELD	FRACT.	74.05 2.06 2.06 1.09 2.01 1.05 1.00 1.00 1.00 1.00 1.00 1.00 1	100.001
DISCARD	LD	cum.	44.01 100.01 100.02	100.00
A A	YIELD	FRACT.	4111122241 8000004201010 00000000000000000000000000000000	100.00
CLEAN COAL	COAL	cum.	88 89 90 90 90 90 90 90 90 90 90 90 90 90 90	100,00
CLEAN	YIELL	FRACT.	88 820000000000000000000000000000000000	100.00
	SPECIFIC		F.1.54 1.54 - 1.56 1.56 - 1.58 1.60 - 1.60 1.60 - 1.60 1.60 - 1.60 1.70 - 1.70 1.72 - 1.72 1.72 - 1.72	TOTAL

TABLE 6. PLANT PERFORMANCE DATA.

i	· · · · · · · · · · · · · · · · · · ·	r	******	.,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	************
MATERIAL	TOTAL	J.6	5.6	4.5	ı
SPLACED MATE	DISCARD	1.0	1.3	2.5	1
MISPL	CLEAN	9.0	1.3	2.1	1
Ę	•	0.014	0,019	0.041	1
CUT	POINT	1.63	1.63	7.64	
ARD	ASH %	42.6	44.0	43.1	39.0
DISCARD	YIELD	10.7	17.2	17.1	1,
COAL	ASH %	12.6	12.0	12.7	13.9
CLEAN (YIELD %	89.3	82.8	82.9	ı
RAW	1 24 OT	15.8	17.5	17.9	16.5
HZIS	FRACTION	4" x 21"	2±" x /8"	x "8/	<u> </u>

TABLE 7.
ANALYSIS OF WEDIUM SAMPLE.

S.G. 1.63
MAGNETIC MATERIAL IN SOLIDS 90.5%
SCREEN ANALYSIS +100 WESH BSS 1.6%
-100 +200 WESH BSS 1.6%
-200 BSS +325 TYLER 4.1%
-325 TYLER 88.6%

ANALYSIS OF MAGNETIC SEPARATOR UNDERFLOW.

SOLIDS CONTENT 27.7 grams per Liter. MAGNETIC MATERIAL IN SOLIDS 2.2%



