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FUEL RESEARCH INSTITUTE

OF SOUTH AFRICA

TEGNIESE MEMORANDUM

NO. 4 OF 1976

A PRELIMINARY INVESTIGATION INTO THE SULPHUR
BALANCE OF A SINGLE-STAGE ANTHRACITE PRODUCER
GAS PLANT

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WORK REQUESTED BY : ANTHRACITE PRODUCERS ASSOCIATION (APA)

- DR K O R GEBHARDT

DIVISION

: ENGINEERING

SECTION

: COMBUSTION

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BALANCE OF A SINGLE-STACE ANTHRACITE PRODUCER

GAS PLANT

1. SYNOPSIS

A two day test has been carried out and it has been shown that approximately 90% of the sulphur in the anthracite was transferred to the product gas.

2. INTRODUCTION

The Institute was asked by Dr K O R Gebhardt, (Consultant to APA), to investigate the sulphur balance of a single-stage gas producer, fuelled with anthracite.

Reserves of low-sulphur anthracite (<17S) in South Africa, are rapidly becoming depleted. APA feel that it is desirable to extend the sale of higher-sulphur anthracite in South Africa and overseas. Many potential customers are in the metallurgical industries, and/or use anthracite-fired producer gas plant, and have processes which are susceptible to a high concentration of sulphur compounds in the gas. Little data are currently available on this subject.

3. BACKGROUND TO TEST

3.1 LOCATION AND DESCRIPTION OF PLANT

Test facilities were granted to APA by Messrs Cullinan Refractories (Pty) Ltd, Olifantsfontein. The plant is a single-stage Wellman Galusha producer. In common with many such plants which are used as a source of process heat, no analytical or quantity monitoring is carried out.

3.2 ESTIMATION OF SULPHUR DISTRIBUTION

As this work was to be of a preliminary nature, it was agreed with Dr Gebhardt that no direct estimation of sulphur in the gas should be carried out, but that this should be obtained by difference. Later, if the results merited it, a full coverage test would be carried out.

The sulphur in the gas has been calculated from weights and analyses of fuel, reject fuel (undersize), ashes and dust. i.e.

S_{FUEL} S_{REJECT} = S_{TO PLANT} = S_{GAS} + S_{ASHES} + S_{DUST}

It was not possible to sample and weigh the fuel to the plant directly.

3.3 FUEL AND ASHES

The anthracite to be used in the test (1 railway wagon) was originally sampled on a falling stream basis at the mine. Unfortunately, however, due to an oversight at Cullinan Refractories, the test fuel was added to the stockpile. A further sample was segregated, weighed and sampled.

The delay between fuel changing and ash discharge was estimated prior to the test by a tracer technique, and the ash sampling was adjusted accordingly.

4. THE TEST

During the test, the plant was run normally by Cullinan Refractories staff, and all readings were taken by FRI personnel.

The fuel was loaded into the empty top hopper of the plant, before the start and the test ended when the hopper was empty with approximately the same level of fuel bed in the generator.

The following data were collected by FRI personnel.

Temperature of product gas

Pressure of product gas

Barometric pressure

Pitot tube differential pressure

Speed of grate

Height of firebed

Every 30 minutes

Blast saturation temperature

Every 2 hours

As appropriate at the beginning or end of the test, fuel, ashes, dust etc were sampled and weighed.

5. RESULTS

5.1 FUEL

** 1 E U.Z.L.		
Size analysis	Fuel elevated	Undersize reject (-6,25 mm)
+ 50 mm	0,57%	
- 50 + 25 mm	58,51%	
- 25 + 12,5 mm	22,71%	
- 12,5 mm	17,79%	
Total weight	28 480 kg	1 588 kg
Proximate analysis		
Calorific value	29,5 MJ/kg	18,8 MJ/kg
Moisture	1,7%	1,3%
Ash	15,0%	45,3%
Volatile matter	10,5%	7,1%
Fixed carbon	72,8%	46,3%

	Sulphur				
	Organic		0,43%		0,35%
	Pyritic	0,15%		0,12%	
	Sulphate	0,02%		0,02%	
	Mineral	0,17%	0,17%	0,14%	0,14%
	Total		0,60%		0,49%
5.2	ASHES AND DUST				
			Ashes		Dust
	Moisture		0,6%		1,2%
	Ash		77,7%		22,7%
	Combustibles		21,7%		76,1%
	Sulphur				
	Organic				0,76%
	Pyritic			0,10%	
	Sulphate			0,02%	
	Mineral			0,12%	0,12%
	Total		0,17%		0,88%
	Total weight		4 511 kg		162 kg

5.3 GAS

Due to the non-availability of a producer gas Orsat, gas analysis could not be carried out. For gas volume calculations, typical figures for a single-stage anthracite producer were used.

Mean blast saturation temperature = 61,0°C.

5.4 TAR

Tar in gas was not measured during the test, but at the request of APA, a single estimation was carried out later. In the method used, a metered volume of gas was passed through a benzene trap and the tar was estimated

gravimetrically.

Volume of gas

Barometric pressure

Metering conditions: pressure
temperature

Tar yield

100 litres
643 mm Hg
14,0 mm w.g.
14,0 mm w.g.

6. DERIVED RESULTS

6.1 ASH BALANCE

Ash to plant = Ash in fuel elevated-ash in rejects
= (0,150 x 28480) - (0,453 x 1588) kg
= 3552,6 kg.

Ash ex plant = Ash in ashes + ash in dust
= (0,77 x 4511) + (0,227 x 162)
= 3541,8 kg.

Percentage accounted for = 99,70%

6.2 SULPHUR BALANCE

Sulphur to plant = Sulphur in fuel elevated - sulphur in rejects

= (0,0060 x 28480) - (0,0049 x 1588)

= 163,1 kg.

Sulphur in gas = Sulphur to plant - (Sulphur in ashes + sulphur in dust)

= 163,1 - ((0,0017 x 4511) + (0,0088 x 162))

= 163,1 - 9,1

= 154 kg.

Percentage of sulphur in coal to gas = 154 x 100 = 94,4%

Note: Sulphur as sulphate in coal = 0.0002×28480 = 5.7 kg.

This is roughly the same order as that calculated for the ashes.

6.3 TAR IN GAS

Tar in gas (from data in 5.4) = 15,56 milligrams/litre at NTP $(15,56 \text{ grams/NM}^3)$.

6.4 GAS VOLUMES (Calculated from pitot readings and ancillary data)

Total gas produced during test $(62,25 \text{ hrs}) = 141 330,5 \text{ NM}^3$ Mean gas production rate = $2270,37 \text{ NM}^3/\text{HR}$.

Thus calculated sulphur content of gas = $\frac{154.0 \times 10^3}{141 \ 339.5}$

= 1,090 grams/NM³

7. CONCLUSIONS

Neither the relatively short period of the test, nor the difference in method used for sulphur estimation is ideal, but the result of 94,4% of sulphur in the coal appearing in the gas is confirmed by the very good ash balance (99,70%).

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DC/MD/ug 1976 March 4th PRETORIA